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Title	Spray-Dried Proliposome Microparticles for High-Performance Aerosol Delivery Using a Monodose Powder Inhaler
Туре	Article
URL	https://clok.uclan.ac.uk/id/eprint/23206/
DOI	https://doi.org/10.1208/s12249-018-1058-4
Date	2018
Citation	Omer, Huner K., Hussein, Nozad R, Ferraz, Amina, Najlah, Mohammad, Ahmed, Waqar, Taylor, Kevin M G and Elhissi, Abdelbary M A (2018) Spray- Dried Proliposome Microparticles for High-Performance Aerosol Delivery Using a Monodose Powder Inhaler. AAPS PharmSciTech, 19. pp. 2434-2448.
Creators	Omer, Huner K., Hussein, Nozad R, Ferraz, Amina, Najlah, Mohammad, Ahmed, Waqar, Taylor, Kevin M G and Elhissi, Abdelbary M A

It is advisable to refer to the publisher's version if you intend to cite from the work. https://doi.org/10.1208/s12249-018-1058-4

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1	Spray-Dried Proliposome Microparticles for High Performance Aerosol
2	Delivery using a Monodose Powder Inhaler
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43 Abstract

44 Proliposome formulations containing salbutamol sulphate (SS) were developed using spray drying, and the effects of carrier type (lactose monohydrate (LMH) or mannitol) and lipid to carrier ratio 45 were evaluated. The lipid phase comprised soy phosphatidylcholine (SPC) and cholesterol (1:1), and 46 47 the ratios of lipid to carrier were 1:2, 1:4, 1:6, 1:8 or 1:10 w/w. X-ray powder diffraction (XRPD) 48 revealed an interaction between the components of the proliposome particles, and scanning electron microscopy (SEM) showed that mannitol-based proliposomes were uniformly sized and spherical, 49 whilst LMH-based proliposomes were irregular and relatively large. Using a two-stage impinger 50 (TSI), fine particle fraction (FPF) values of the proliposomes were higher for mannitol-based 51 formulations, reaching 52.6%, which was attributed to the better flow properties when mannitol was 52 used as carrier. Following hydration of proliposomes, transmission electron microscopy (TEM) 53 54 demonstrated that vesicles generated from mannitol-based formulations were oligolamellar, while 55 LMH-based proliposomes generated "worm-like" structures and vesicle clusters. Vesicle size decreased upon increasing carrier to lipid ratio, and the zeta potential values were negative. Drug 56 57 entrapment efficiency (EE) was higher for liposomes generated from LMH-based proliposomes, reaching 37.76% when 1:2 lipid to carrier ratio was used. The in vitro drug release profile was similar 58 59 for both carriers when 1:6 lipid to carrier ratio was used. This study showed that spray drying can produce inhalable proliposome microparticles that can generate liposomes upon contact with an 60 aqueous phase, and the FPF of proliposomes and the EE offered by liposomes were formulation-61 dependent. 62

63 *Key words:* Aerosol; Morphology; Particle size; Powder; Pulmonary

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70 1. Introduction

Inhalation of therapeutic materials in liposome formulations has been studied as a strategy for 71 controlled drug release in the lungs. There is evidence that liposomes can retain the drug in the 72 73 pulmonary tissues for prolonged periods, reducing the need for frequent dosing and minimizing the potential of systemic adverse effects (1-5). Many studies have investigated the pulmonary delivery 74 75 of relatively large volumes of liposome dispersions using medical nebulizers (1,6,7). There are at 76 least two nebulizable liposome formulations currently in clinical trials for potential approval in the treatment of pulmonary infections, for example, Arikace® (liposomal Amikacin) for the treatment of 77 pseudomonas aeruginosa in cystic fibrosis patients (7,8), and Pulmaquin® (liposomal ciprofloxacin) 78 for the treatment of non-cystic fibrosis lung infections (9). 79

80 Although nebulization is the most studied means of delivering liposomes by inhalation, there are a number of disadvantages associated with using nebulizers for this purpose. First, liposome instability 81 caused by shearing during nebulization and concomitant losses of the originally entrapped drug is a 82 major challenge, necessitating extensive work to engineer the optimal liposome size and bilayer 83 84 composition, and select nebulizers with appropriate designs and operating parameters (7,10). Second, the performance of the aerosol (e.g. output, droplet size, 'FPF', etc.) generated from these nebulizers 85 is greatly influenced by the physicochemical properties of formulation (11,12), which means that 86 nebulizer performance for one liposome dispersion may not be the same for another formulation (13). 87 88 Third, the large volumes delivered via nebulizers may contribute to toxicity not only by the drug but also by the accompanying excipients. For example, in pulmonary infections, inhalation of relatively 89 large antibiotic doses is needed to eradicate the infection, necessitating the use of large phospholipid 90 quantities to entrap the antibiotic and sustain its release. In spite of the established biocompatibility 91 and biodegradability of liposomes, dose-limiting toxicity of phospholipids in animals has been 92 93 reported (14).

94 Dry powder inhalers (DPIs) offer the advantages of delivering small doses of drug and excipients, and avoidance of shearing-induced liposome instability during delivery. Compared to the number of 95 studies published for the delivery of liquid liposome dispersions via nebulization, a limited number 96 97 of reports have attempted to explore the potential of liposomes and phospholipid formulations for pulmonary applications delivered in the dry powder form. It has been postulated by several 98 investigators that dried liposomes would exploit the aqueous environment of the lung to be hydrated 99 in situ within the respiratory tract (5). Freeze-drying of liposomes in the presence of a cryoprotectant 100 101 followed by micronization has been studied for the generation of inhalable dry powder liposomes; 102 however, milling may exert a deleterious effect on vesicle stability, causing leakage of the drug upon rehydration (15,16). As an alternative to freeze-drying (lyophilization), spray-drying of liposomes 103 dispersed in carbohydrate solutions has been investigated, with high powder 'respirability' being 104 105 reported in a range of studies (17-21).

106 As an alternative to traditional liposome powders, particulate proliposome formulations have been 107 developed for inhalation. Proliposomes are carbohydrate carriers coated with phospholipid to generate liposomes upon addition of aqueous phase (22,23). Proliposomes, in the context of this 108 study, are phospholipid and drug blended with diluent carbohydrate carriers, aiming to generate 109 liposomes upon contact with the pulmonary physiological milieu (5). In one approach, phospholipid 110 and drug were mixed with lactose followed by air-jet milling. The resultant proliposome blend 111 generated multilamellar vesicles (MLVs) upon dispersion in aqueous phase, with entrapment 112 113 efficiencies (24) and fine particle fractions (FPF) (25) being dependent on formulation. Spray drying 114 of alcoholic phospholipid solutions may also generate proliposome particles (26-28) with FPFs in the range of 20-30% using antibiotics such as pyrazinamide (28). Thus, the potential of inhalable 115 116 proliposome powders has been explored for delivering antimicrobial drugs. Although the antibacterial activity of hydrated proliposome has been established in vitro (27), the need for large doses for the 117 eradication of lung infections in vivo raises doubts about the suitability of DPIs in delivering 118 therapeutic amounts of antimicrobial agents. Unlike pulmonary infections, the doses needed to treat 119

asthma are very small, hence powdered formulations (e.g. in the form of proliposomes) canpotentially be used as antiasthma delivery systems.

In this study, we have introduced a potentially applicable approach for pulmonary delivery using 122 spray-dried proliposomes loaded with salbutamol sulphate (SS). Proliposomes consisted of 123 carbohydrate carriers (lactose monohydrate or mannitol) and lipids (soya phosphatidylcholine and 124 125 cholesterol; 1:1) were formulated using a range of lipid to carriers ratios. The resultant proliposome powders were thoroughly characterized, and using a two-stage impinger (TSI), the deposition of the 126 drug was evaluated following proliposome delivery from a Monodose inhaler device. Furthermore, 127 128 the ability of the proliposomes to generate liposomes following hydration was studied and drug 129 entrapment was determined, to evaluate the potential of the formulations in providing a reservoir, in situ, for sustaining the drug release. The findings of this study using proliposomes were evaluated in 130 131 light of the progress achieved in the field of pulmonary delivery of dry powder formulations.

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133 2. Materials and methods

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135 2.1 Materials

Lactose monohydrate (LMH) was purchased from VWR, UK, and D-mannitol and cholesterol (CH)
were bought from Sigma Aldrich, UK. Solvents used in HPLC experiments including Water and
methanol were HPLC-grade and HPLC-grade 99.9%, respectively and were supplied by Fisher
Scientific, UK. Absolute ethanol and ethanol (96%) were also purchased from Fisher Scientific, UK.
Sodium 1-hexane sulfonate monohydrate (99%), acetic acid glacial (99%) and salbutamol sulphate
(SS; 99%) were purchased from Alfa-Aesar, UK. The phospholipid used, namely soya
phosphatidylcholine (SPC; Lipoid S-100) was kindly gifted by Lipoid, Switzerland.

143 2.2 Methods

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145 2.2.1 Spray drying of mannitol and LMH

Carbohydrate carriers (LMH or mannitol) were spray-dried by dissolving the carrier particles in distilled water (1% w/v), followed by spraying the carbohydrate solution through the spray-drier's nozzle (diameter = 0.7 mm) using a B-290 spray drier (Büchi, Switzerland). The inlet temperature was set at 130°C, spraying flow rate was 600 L/h, feed rate was 17%, and the outlet temperature was $70 \pm 2^{\circ}$ C. The resultant spray-dried microparticles were used as core carriers to prepare particulatebased proliposomes. This step of spray drying aimed for enhancing the dispersion of the carbohydrate carriers in ethanol during the preparation of proliposomes, as described in the subsequent section.

153 2.2.2 Manufacture of particulate-based proliposome particles via spray drying

The constituents used to prepare proliposomes are demonstrated in Table 1. Spray-dried mannitol or 154 155 LMH microparticles were employed as core carriers for manufacturing proliposomes. This was achieved by weighing a total of 100 mg lipid consisting of SPC and CH (1:1 mole/mole), followed 156 157 by addition of 100 mL ethanol (96% grade), and SS (10 mg). The alcoholic mixture was sonicated for 1 min to aid complete dissolution of lipids in ethanol. The spray-dried mannitol or LMH in various 158 ratios were dispersed in the ethanolic solution followed by sonication for 15 min to break up any 159 agglomerates of the carbohydrate particles before performing spray drying using the same Buchi B-160 161 290 Mini Spray Dryer equipment, but this time connected with the Buchi's inert loop system (Buchi, 162 Switzerland). The homogeneity of the resultant alcoholic mixture was maintained by continuous stirring while feeding the mixture into the spray drier. The spray drying conditions were optimized 163 164 by adjusting the inlet temperature at 120°C, spray flow rate was 600 L/h, feed rate was 11% and the outlet temperature was $73 \pm 3^{\circ}$ C. The resultant powder constituting lipid/carbohydrate was collected 165 166 and referred to as 'proliposomes', which were stored in a desiccator for later use in the same day.

168 2.2.3 Hydration of spray-dried powder

Samples of spray-dried powders were hydrated by adding deionized water followed by vortex mixing for 2 min in order to test for the possible generation of liposomes. The liposome dispersion was allowed to "anneal" for around 1 h at room temperature before performing further characterization. Allowing the liposomes to anneal at temperatures above that of the lipid phase transition (T_m) may promote the stability of liposomes by overcoming structural defects of the bilayers [29].

174

175 2.2.4 Product yield estimation

The product yield (*PY*) of spray-dried powders was determined using the weight of the final spraydried powder (W°) divided by the initial weight of carrier, lipid and drug employed (*WT*). The product yield, drug recovery and content drug uniformity were determined according to the following equations (30):

180
$$PY(\%) = \frac{W^{\circ}}{WT} \times 100 \qquad Eq. 1$$

181

182
$$Drug recovery (\%) = \frac{P_W}{WT} \times 100$$
 Eq. 2

183 Where Pw is the practical weight of the drug after spray-drying was performed, as quantified using

184 high performance liquid chromatography (HPLC).

185 Content drug uniformity (%) =
$$\frac{Drug recovery (\%)}{PY (\%)} \times 100$$
 Eq.3

186

187 2.2.5 Scanning electron microscopy (SEM)

Particle size and morphology of spray-dried formulations were studied using scanning electron
microscopy (SEM, Quanta-200, FEI at 20 kV). Spray-dried particles were spread onto an aluminium
stub and coated with a film of gold using the JFC-1200 Fine Coater (JEOL, Tokyo, Japan).

191

192 **2.2.6 X-ray powder diffraction (XRPD) studies**

193 X-ray diffraction (XRPD) studies of powder were performed by utilizing the Equinox 2000 (Inel, 194 France) using a diffracted-beam monochromator with Cu radiation. The intensity of diffractions was 195 recorded at an angle of 2-theta, at a diffraction scan duration of 20 min. The experiments were 196 conducted by keeping the voltage at 32 kV and the current generator at 28 mA.

197

198 2.2.7 Studies of vesicle morphology using transmission electron microscopy (TEM)

A drop of hydrated spray-dried powder was carefully positioned on carbon-coated copper grids (400
mesh; TAAB Laboratories Equipment Ltd., UK), followed by negative staining (using 1%
phosphotungstic acid; PTA). The samples were imaged using the Philips CM 120 Bio-Twin electron
microscope (Philips Optics BV, the Netherlands).

203

204 2.2.8 Particle size measurements of hydrated samples

Size and size distribution of liposomes generated upon hydration of spray-dried proliposomes were analysed by laser diffraction using the Mastersizer 2000 (Malvern Instruments Ltd., UK). The median size, also referred to as volume median diameter (VMD; 50% undersize), and Span were measured to represent the size and size distribution (polydispersity) of liposomes, respectively. Span value

represent the difference between 90% undersize and 10% undersize divided by the VMD. Span is aunit-less term introduced by the manufacturer of the Malvern Mastersizer 2000 instrument.

211

212 2.2.9 Zeta potential measurements

The zeta potential of vesicles was determined via the Zetasizer Nanoseries instrument (Malvern Instruments Ltd., UK) by choosing the relevant software option of the instrument. Proliposomes were hydrated with deionized water with shaking. The resultant liposomes (70 μ L) were loaded via a Gilson pipette into the Malvern's zeta potential cells, after setting the temperature at 25°C and allowing 2 min for sample equilibration in order to obtain consistent zeta potential measurements.

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219 2.2.10 Drug content and entrapment efficiency (EE) studies

220 Spray-dried powder (10 mg) was dispersed with deionized water (1 mL) to generate liposomes. The dispersion was transferred into a volumetric flask (10 mL), and methanol (1 mL) was added to 221 222 dissolve the lipid followed by making up the volume with water. HPLC was employed to determine 223 the drug content in the flask (i.e. total drug loaded into the 10 mg powder sample) by adapting a method we published established (13). The mobile phase was made by making a buffer solution 224 constituting a mixture of sodium hexane sulfonate in water (5 mM) and methanol (75:25 v/v), to 225 226 which glacial acetic acid was added to have 1% of the total volume. The high-performance liquid 227 chromatography (HPLC; Agilent 1200 - UV detector system; Hewlett-Packard Co., USA) was set up with a Symmetry C-18 column (150 mm, 4.6 mm, 5m; Waters, UK). The samples (injection volume 228 229 of each is 20 μ L) were analysed at 276 nm. The flow rate of mobile phase was set up at 1 mL / min at 40 °C. To determine the entrapment efficiency (EE), spray-dried powder (10 mg) was hydrated 230 using deionized water (50 µL) followed by vortex mixing for 2 min and dilution with deionized water 231 (950 µL). The liposomes were left for 1 h at room temperature to anneal, followed by further dilution 232 233 to 8 mL with deionized water. The liposomes were then centrifuged at 55,000 rpm (277,000 x g) for

35 min at 6°C (Beckman LM-80 ultracentrifuge; Beckman Coulter Instruments, USA). The
supernatant was aspirated for subsequent analysis of SS (the unentrapped fraction of drug). The EE
was determined using the following equation:

237

238
$$EE(\%) = \frac{Total \ drug \ loading - Unentraped \ drug}{Total \ drug \ loading} \times 100 \qquad Eq.4$$

239 2.2.11. In vitro drug release study

240 The release of SS from liposomes generated from the proliposome powders was investigated using the dialysis method. Spray-dried powder (71 mg containing 1 mg SS) was dispersed with deionized 241 242 water (0.5 mL) followed by vortex mixing for 1 min and dilution with deionized water (1.5 mL) to generate liposomes. The dispersion was placed in a dialysis tube (MWCO 3500) and tightly sealed. 243 For free drug, 1 mg SS was dissolved in 1 ml of ethanol: water: tween 80 (20:79.9:0.1%). Then, the 244 dialysis tube was immersed in 50 mL (total volume) release medium (deionized water) containing 245 0.1% (v/v) Tween 80) and incubated with stirring in for 24 h at 37°C. Samples (0.3 mL) were taken 246 247 at time intervals from the release medium for 24 h, and replaced by a similar volume of fresh medium. The concentration of SS was determined by HPLC using the methods described above. 248

249

250 2.2.12 Assessment of aerosol performance in vitro

Using the Two-Stage Impinger (TSI), also called the Twin Impinger or the Single Stage Glass 251 Impinger (Copley Scientific Ltd, Nottingham, UK), the performance of spray-dried proliposome 252 aerosols and deposition profile were investigated (31) using a Miat Monodose powder inhaler (Miat, 253 Italy). TSI is designed with two stages: the upper stage (S1) and the lower stage (S2), attempting to 254 represent the upper airways and lower airways, respectively. The flow rate through the TSI was set 255 256 up at 60 L/min. The cut-off aerodynamic diameter between the two stages at 60 L/min is 6.4 µm, hence particles smaller than this aerodynamic diameter will most likely deposit in the lower impinger 257 and will constitute the 'fine particle fraction' ('FPF') (31). Proliposome powder (25 mg) was filled 258

259 into hydroxypropyl methylcellulose (HPMC; size 3) capsules. Each capsule was loaded into the Miat 260 device which was then connected to the impinger that contained deionized water as collection medium (7 mL in the upper stage (S1) and 30 mL in the lower stage (S2). In each experiment, the 261 262 capsule content was pulled by applying negative pressure (60 L/min) through the actuated inhaler 263 device over 5 s. Then, the impinger was dismantled and each stage, the inhaler device and capsule were separately rinsed with deionized water for subsequent drug quantification using HPLC. The 264 total amount of drug in the inhaler device, S1 and S2 constitutes the recovered dose (RD) of the drug. 265 266 The amount of drug deposited in S1 and S2 of the impinger constitutes the emitted dose (ED) calculated as the percentage proportion of the RD (Eq. 5). The percentage proportion of the drug that 267 is deposited in S2 of the impinger was calculated as the "FPF" (Eq. 6). 268

$$ED = \frac{S1 + S2}{RD} \times 100 \qquad Eq.5$$

$$FPF = \frac{S2}{RD} \times 100$$

271

272 2.2.13 Proliposome flowability studies

273 Aiming to understand the behaviour of selected formulations, the bulk density of the spray-dried 274 proliposome powder was measured by using the ERWEKA tapped density meter (ERWEKA®p 275 Gmbh, D-63150 Heusenstamm, Germany). A defined mass of powder was poured into a calibrated 276 measuring cylinder and the volume occupied by the powder was recorded. The tapped density of 277 spray dried powder was determined by volume measurement of the tapped mass until no further changes in the powder volume were observed. Hausner ratio and Carr's index, also called Carr's 278 279 compressibility index, for each spray dried powder were derived according to the following 280 equations:

Eq.6

$$BD = \frac{W}{V} \times 100 \qquad Eq. 7$$

282
$$TD = \frac{W}{Vt} \qquad Eq.$$

Hausner Ratio = $\frac{V}{Vt}$ Eq.9

$$Carr's Index = [1 - \left(\frac{BD}{TD}\right)] \times 100$$
 Eq.10

Where BD and TD are bulk density and tapped density, respectively, and V and Vt are actual volumeand tapped volume, respectively.

287

288 2.2.14 Statistical analysis

All experiments were conducted three times using three different proliposome batches. Statistical significance was studied using one-way analysis of variance (ANOVA) and student's *t*-tests, for comparing more than two sets and two groups of results, respectively. P values < 0.05 indicate that difference between compared groups is statistically significant.

293

294 3. Results and discussion

295 **3.1 Product yield and drug content uniformity of spray-dried proliposomes**

Table 2 shows the product yield (PY), drug recovery and drug content uniformity of powder formulations. Since spray-drying conditions were the same for all formulations, any difference in PY was attributed to formulation composition, namely, carrier type and lipid to carrier ratio. Spray-drying parameters such as atomizer design, flow rate and temperature of the drying air, solid content of the feed solution can all influence PY of spray-dried powder (32).

For both carriers, a direct relationship was observed between PY and carrier concentration (Table 2). PY of F1 was lower than F2 (p<0.05), and PY of F2 was lower than F3, F4 and F5 (p<0.05) (Table 2). However, when PY values of F3, F4 and F5 were compared, the difference was not significant statistically (P>0.05). Moreover, PY of F6 was significantly (p<0.05) lower than PY of F7 which, in turn, was significantly (p<0.05) lower than PY values observed with F8, F9 and F10. Only a trend of higher PY was also found for F9 and F10 when compared to F8 (p>0.05) (Table 2). The decrease in

PY of spray-dried formulations is attributed to possible adherence of the sprayed droplets and dry particles to the inner walls of the drying compartment, or because of poor collection of fine powder by the cyclone separator [33]. Thus, the high lipid content of F1, F2, F6 and F7 can be responsible for the low PY of these formulations, causing adherence of lipid to the inner walls of the drying compartment.

312 The PY of LMH formulations (F6, F7, F8, F9 and F10) was generally higher than PY of proliposomes 313 based on mannitol carrier (F1, F2, F3, F4 and F5), indicating that it is not only lipid content that can affect PY but also carrier type (Table 2). Other reports have demonstrated that glass phase transition 314 315 (Tg) of carbohydrates has a prime effect on the behaviour of formulations during spray drying (34-316 37). When the temperature during spray drying is higher than T_g of the sugar employed, adherence of formulation components on the walls of the drying chamber may increase, resulting in lower 317 318 powder yields (38). The Tg of lactose is 101°C (39,40) which is higher than the outlet temperature 319 used in the present study, whilst Tg of mannitol is lower than the outlet temperature used (41-44), 320 making mannitol-based proliposomes more adhesive with concomitant lower PY than LMH-based formulations (Table 2). 321

Table 2 also shows the recovery values of salbutamol sulphate (SS). The recovery of drug increased 322 with increasing the carrier ratio in the proliposomes, regardless of carrier type. The enhanced drug 323 324 recovery is paralleled with the higher PY obtained when higher carrier ratios (i.e. lower lipid 325 concentrations) were used. Thus, low drug recovery for F1, F2, F6 and F7 formulations is attributed to the incorporation of high lipid contents. Table 2 also shows drug content uniformity in the spray-326 327 dried proliposomes, which was in the range of 90 - 109%, indicating uniform distribution of SS in the powder. Drug content uniformity using LMH carrier was higher than formulations based on 328 329 mannitol carrier (Table 2). In an attempt to provide the reasons behind these differences, particle morphology of proliposomes was investigated as illustrated in the subsequent section. 330

332 3.2 Morphology of spray-dried proliposome particles

333 Particle morphology of proliposomes presented in Table 1 was studied using SEM (Figure 1). 334 Mannitol-based particles looked spherical regardless of lipid to carrier ratio (Figure 1), coming in 335 agreement with previous investigations employing this carrier (26). Particles of F1 and F2 were spherical and had small sizes, and apparently smooth surfaces, and tended to form large agglomerates 336 (Figure 1a, b). The agglomeration of these two formulations can be attributed to their high lipid 337 content, and may justify their low PY values (Table 2), making their potential for 'deep lung' 338 339 deposition questionable. By contrast, F3 particles were small, porous and spherical, with less propensity to form agglomerates (Figure 1c). Porosity of particles can enhance their aerosol 340 performance (45). F4 and F5 were small and spherical with apparently smooth surfaces and evidence 341 342 of particle agglomeration (Figure 1d, e), possibly due to high surface energy of the particles, which 343 commonly increases cohesiveness and compromises flowability (46-48).

By contrast, LMH-based proliposome microparticles were irregular, rough and not similar in size (Figure 2). LMH is practically insoluble in ethanol used as the solvent in the present investigation. Upon atomization during spray drying, it appears that ethanol did not form uniform droplets; hence, the resultant proliposome particles had an irregular shape and wide size distribution. Studies have correlated particle surface morphology with aerosol performance (49). Smooth particles have high flowability and are potentially applicable for aerosolization (50). The irregular shape and rough surface of lactose microparticles can promote the interaction between carrier and drug (49).

Particles that have spherical shape may have high chance for deposition in the peripheral airways, especially when the aerodynamic size is in the range of 1-5 µm (51-54). Thus, LMH-based proliposomes might have lower suitability for delivery from DPI devices than mannitol-based formulations, since LMH-based particles are larger and more irregular in shape (Figure 2). According SEM, the potentially most appropriate proliposome formulation for use as DPIs would be F3 (i.e. using mannitol carrier with 1:6 w/w lipid to carrier ratio) (Figure 1c).

357

358 **3.3 Crystallinity of spray-dried formulations**

XR diffraction profiles of SS are shown in Figure 3. The intensity of drug peaks before and after spray drying indicates that the crystalline characteristics of SS were preserved. The intensity peak after spray drying increased slightly, because ethanol can increase powder crystallinity (55-58). Mannitol had high crystallinity before spray drying (Figure 3c); however, the peak intensity decreased by spray drying (Figure 3d), indicating reduced crystallinity of this sugar (59). High amorphous content of solids can facilitate dispersion of powder in aqueous media (60-62), which is advantageous in dry powder formulations.

Spray-dried mannitol is crystalline (Figure 3d). The X-ray diffraction profile of the drug was not detected in the proliposome formulations (Figure 4; Figure 6), because of the low drug concentration when compared to the other formulation components (i.e. mannitol and lipid). Moreover, the drug might have been coated by SPC that is known to be amorphous, resulting in poor detection of crystalline drug traces. Similarly, DSC curve of the formulation F3, for example, did not show a thermogram for the drug. However, the pure drug shows an endothermic melting peak with the onset of about 200°C.

373 The X-ray diffraction patterns of mannitol proliposomes are presented in Figure 4. The crystalline characteristics of mannitol were dominant in all formulations because of the high content of sugar 374 compared to the other components of the formulations (i.e. drug and lipid). X-ray diffraction profile, 375 as evident from the intensity of the main peak of mannitol-based proliposomes was formulation-376 377 dependent, when F1-F5 formulations were considered. The intensity of the main peak increased 378 slightly by increasing the ratio of mannitol, owing to the high crystallinity of this type of sugar. The 379 intensity peak of mannitol-based proliposomes (F1-F5) was lower than mannitol alone, indicating 380 other formulations components (mainly the lipid) have decreased powder crystallinity.

381 Figure 5 shows the X-ray diffraction profiles of LMH before and after spray-drying in aqueous or 382 alcoholic solutions. As shown in Figure 5a, LMH demonstrated a crystalline profile before spraydrying (Figure 5a), and converted into amorphous because of spray-drying in aqueous solution 383 384 (Figure 5b), agreeing with previous reports employing this type of sugar (63-67). By contrast, LMH preserved its crystallinity after spray drying from its ethanolic solution, possibly because of the lower 385 solubility of this sugar in ethanol when compared to its aqueous solubility. However, the intensity 386 peak of LMH was diminished by spray drying from ethanol compared to before spray drying (Figure 387 388 5c). LMH is crystalline in all formulations due to the high sugar content, regardless of formulation 389 (Figure 6); however, slight differences in the intensity of the main peak was observed when the formulations F6-F10 were compared. Thus, crystallinity increased slightly with increasing LMH ratio 390 391 in the formulation.

The DSC thermographs for F3 and F8 conformed the preserved crystallinity of both mannitol and LMH, respectively, after spray-drying from ethanolic solution. However, no peaks appeared for the drug in both formulations thermograms (data not shown).

395 3.4 Drug entrapment in liposomes generated upon hydration of spray-dried proliposomes

396 Drug entrapment efficiency (EE) in liposomes was determined after hydration of the proliposome 397 powder (Table 3). For mannitol-based proliposomes, entrapment differed slightly for different formulations (Table 3). This can be attributed to different proportions of lipid recovered after spray 398 399 drying, or difference in morphology of proliposome microparticles with accordance to using different formulations. Rough carrier particle surfaces may facilitate carrier-drug interactions due to having 400 401 high surface area, whilst smooth surfaces may result in loose interactions between the drug and carrier (49,68,69). Thus, the apparently rough surfaces of LMH-based formulations could be responsible for 402 enhanced drug-carrier interactions, facilitating drug encapsulation by liposomes upon hydration. This 403 explains the higher drug entrapment in vesicles generated upon hydration of LMH-based 404 405 proliposomes compared to mannitol-based formulations (Table 3). Furthermore, F6 and F7 (i.e. lower 406 LMH content; higher lipid proportion) had greater drug entrapment efficiencies than F8-F10 (i.e.

407 higher LMH content; lower lipid content) formulations. Thus, the relatively low lipid concentrations 408 in F8, F9 and F10 caused the generation of dilute liposome dispersions; thus, lower drug proportions 409 were encapsulated by the vesicles (Table 3). LMH-based proliposomes with 1:2 lipid to carrier ratio 410 (i.e. F6 formulation) gave the greatest drug entrapment efficiency, because of the high lipid content in this formulation. These findings demonstrated a correlation between PY, particle morphology and 411 drug entrapment efficiency. Other investigators have hypothesized possible hydration of proliposome 412 powders in situ within the lung after inhalation by exploiting the aqueous physiological environment 413 of the lung (24-28). In vivo investigations are merited in the future to explore the validity of this 414 hypothesis. Our ongoing studies involving the use of simulated lung fluids to explore the potential of 415 dehydrated liposome and proliposome formulations when the hydration environment is made from 416 417 aqueous systems other than simple solutions are supportive to the aforementioned hypothesis (results 418 unpublished).

419

420 3.5 Size analysis of hydrated proliposomes

The volume median diameter (VMD), also referred to as median size, of liposomes after 421 reconstitution of the powders in deionized water was in the range of 3.38 - 6.01 µm and 3.23 - 5.96 422 µm for mannitol-based vesicles and LMH-based liposomes, respectively (Table 3). Liposome size is 423 an influential factor on drug entrapment, retention time of the vesicle components in the lung, and 424 425 drug release profile (70). F1 and F6 had the largest VMD measurements and highest drug entrapment efficiencies, whilst F4 and F10 had the smallest VMD values and lowest drug entrapment 426 427 measurements (Table 3). The high lipid content in F1 and F6 could be responsible for generating the largest vesicles that demonstrated the highest drug entrapment efficiencies. Drug release and 428 absorption of liposome-encapsulated drug are influenced by liposome size and lipid phase 429 composition. For instance, the localized time of terbutaline in the pulmonary system was prolonged 430 431 by enriching the liposome formulations with CH or by using phospholipids with saturated alkyl chains 432 (71). Large liposomes and multilamellarity can promote drug entrapment and prolong drug release in

the lung (72). The Span measurements were approximately 2 or less except for F4, F8 and F9 (Table
3), indicating different polydispersity for different formulations. The high Span values (i.e.
polydispersity) could be due to aggregation of liposomes.

436

437 **3.6 Zeta potential measurements**

Particles with a net surface charge (negative or positive) may repel each other, causing lower tendency for aggregation during storage, which improves physical stability of formulation stability (73). Furthermore, surface charge on particles, especially negative charge, may influence the interaction of particles with biological membranes (74-76). Liposomes in all formulations had very slightly negative zeta potential values (Table 3), indicating that lipid to carrier ratio, and carrier type did not affect the surface charge of vesicles. These findings support the potential of our liposome formulations, as particles with negative charge may demonstrate enhanced cellular uptake (74-76).

445

446 3.7 Studies of vesicle morphology using transmission electron microscopy (TEM)

Liposomes generated upon hydration of mannitol-based proliposomes were a mixture of large 447 unilamellar (LUVs) and oligolamellar vesicles (OLVs), while structures generated from LMH-based 448 449 powders were rich of vesicle clusters and "worm-like" shapes (Figure 7). These findings are in agreement with one of our previous investigations, for liposomes generated from LMH-based 450 proliposomes manufactured using a modified rotary evaporator (77). Based on this TEM study, 451 liposome morphology was unaffected by other formulation factors such as lipid to carrier ratio or 452 lipid composition. The slow dissolution of carrier, may slow the hydration of lipid, resulting in 453 retarded deaggregation of vesicles and formation of elongated bilayer structures (77). By contrast, 454 455 mannitol-based proliposomes may have better dispersion properties in water, which might be due to 456 the small size, smooth surfaces and spherical shape of mannitol-based particles, as shown earlier by SEM (Figure 1), causing formation of spherical LUVs and OLVs (Figure 7). Thus, the different in 457

458 hydration patterns of phospholipid because of using proliposomes with different morphologies 459 resulted in generation of vesicles with different morphologies (Figure 7). Interestingly, previous 460 studies employing traditional proliposomes manufactured using modified rotary evaporators revealed 461 instant generation of liposomes upon hydration of proliposomes under static conditions (i.e. without 462 shaking) via the 'budding off' mechanism (22, 23, 77). Further studies should investigate the role of 463 carrier type on the behaviour of liposomes generated from proliposomes.

464

465 **3.8 Powder aerosolization performance** in vitro

Proliposome with spherical shapes would be expected to have better flowability, and when combined 466 with having small particle size (i.e. in the 'respirable' range), they become likely to deposit in the 467 468 lower airways. However, SEM used to evaluate particle morphology does not give information about aerodynamic size. The deposition site of inhaled particle in the pulmonary system is influenced by 469 particle shape and aerodynamic size (78). For this reason, inertial impaction studies using the two-470 stage impinger (TSI) were conducted. Using the MIAT inhaler device, deposition of proliposome 471 472 particles in the stages of the TSI was studied, in order to determine the recovered dose (RD), emitted 473 dose (ED) and 'FPF' (Figure 8).

Figure 8 shows that the performance of proliposome aerosols was dependent on carrier type and lipid to carrier ratio (Figure 8). The RD for all formulations approached 100% (95.62 – 99.79%), with higher values for LMH-based proliposomes than mannitol-based formulations (p<0.05)However, the delivery of coarse LMH-based proliposome particles from the capsule was better (i.e. ED was higher) than ED of mannitol-based proliposomes.

The ED was high for all formulations (77.46 – 94.59%). However, LMH-based proliposomes had higher deposition in the upper stage (S1) of the impinger (i.e. lower 'FPF'). These findings are in agreement with the earlier SEM studies, since all LMH-based proliposome formulations (F6-F10) (shown to have large sizes and irregular shapes; Figure 2) had extremely poor 'FPF' (0 - 3.99%)

483 (Figure 8). By contrast, mannitol-based microparticles were smaller and more spherical (Figure 1). Hence, they offered much greater 'FPF' (2.79 - 52.14%) compared to LMH-based powder. Particles 484 485 having size of 1-5µm are likely to reach the peripheral airways following inhalation (51). F1 had the 486 lowest FPF amongst mannitol formulations, which can be ascribed to particle agglomeration due to the high lipid content of this formulation. For F2 and F5, the 'FPF' values were 33.57 and 33.63%, 487 respectively. These values were lower than those determined for F3 and F4, which can be attributed 488 to the agglomeration occurring in F2 and F5 formulations because of the presence of small particles. 489 490 By contrast, the lower agglomeration tendency of F3 and F4 might be responsible for the enhanced deposition of particles into the lower stage of the TSI (Figure 8). The subsequent section elaborates 491 on studying the characteristics of proliposomes and the generated liposomes, using two distinguished 492 493 formulations with superior aerosol performance.

494

495 **3.9.** Additional powder characterization and drug release studies

496 Further powder characterization studies and drug release investigations were conducted on best 497 performing proliposome formulations, mainly relaying on the aerosol performance findings of the powders (Figure 8). Proliposome powders exhibited their best performance in terms of 'FPF' when 498 499 the lipid to carrier ratio was 1:6; thus F3 (mannitol-based proliposomes) and F8 (LMH-based proliposomes) were further investigated in terms of powder flowability and moisture content, and the 500 501 release profile of SS from the subsequently generated liposomes. Upon reflection on the earlier findings in this study, it was further observed that F3 and F8 formulations exhibited desirable 502 503 characteristics in terms of drug recovery, PY and drug content uniformity (Table 2). Moreover, as observed earlier with SEM studies, F3 proliposomes were spherical and apparently smooth with low 504 agglomeration propensity (Figure 1c), justifying the superior aerosol performance of this formulation 505 (Figure 8) and supporting the rationale behind conducting flowability and drug release studies on this 506 507 particular proliposome composition.

508 Accordingly, flowability studies were conducted on both F3 (as representative for mannitol-based 509 proliposomes) and F8 (as representative for LMH-based formulations). Spray-dried powders of 510 mannitol and LMH were used for comparison with the proliposome formulations to investigate the 511 effect of lipid on powder flowability (Table 4). Flowability was assessed using Carr's compressibility index and Hausner ratio according to the reference published in 1965 (79) and summarized in Table 512 4. Lipid-free carriers (i.e. spray-dried powders of mannitol or LMH) exhibited 'Fair' flowability 513 according to both Hausner ratio and Carr's index (Table 4; Table 5). When these carriers were used 514 515 to manufacture spray-dried proliposomes (i.e. F3 as a representative for mannitol-based formulations, and F8 as a representative for LMH-based formulations), the flow characteristics were markedly 516 compromised, so that F3 exhibited 'Poor' flowability, whilst F8 was regarded to have 'Very very 517 poor' flowability according to both Hausner ratio and Carr's index (Table 4; Table 5). Although the 518 519 flowability findings do not look encouraging for both proliposome formulations (F3 or F8), the 520 emitted dose (ED) of SS from the capsules to the impinger was considerably high, exceeding 80% (Figure 8), indicating that the 'inspiratory' flow rate through the impinger was sufficiently powerful 521 522 to pull the proliposome powders from the inhaler device. However, the relatively better flow 523 characteristics of F3 (Table 5) in addition to the spherical morphology, the relatively small physical size, and apparent smooth surfaces of this formulation (Figure 1c) were the prime reasons for the 524 superior 'FPF' value observed for F3 (Figure 8). By contrast, F8 demonstrated very poor 'FPF' 525 526 (Figure 8), possibly due to the relatively large size, irregular shape and rough surfaces (Figure 2c) and the extremely poor flow properties of the particles (Table 5). The flow rate through the impinger 527 528 was appropriate to aspirate a large dose of F8 particles, but most of the drug dose was deposited in 529 the upper impinger, resulting in extremely poor 'FPF' values (Figure 8). Particle surface morphology can influence aerosol performance (49) and smooth particles may exhibit better aerosolization 530 characteristics (50). It is worth to mention that the residual moisture contents for both formulations 531 532 F3 and F8 were less than 0.8% as determined by thermogravimetric analysis (TGA) at 110°C (data

533 not shown). TGA is a well-established analytical tool for the determination of residual moisture 534 content in powdered formulations and solid excipients (80, 81).

When the in vitro drug release profiles of F3 and F8 were compared, the difference was insignificant for most intervals studied (p >0.05); however, a trend for faster drug release was observed with the F3 formulation (Figure 9). After 24 h, the cumulative release for SS was 79% and 72% for F3 and F8 formulations, respectively, demonstrating advantageous sustained release for both formulations in comparison to the free SS which demonstrated 93% cumulative release after as short as 8 h and full release after 24 h (Figure 9). The drug release findings of F3 and F8 indicate that carrier type (mannitol or LMH) had no significant influence on the drug release profile.

542

In our opinion, if nebulizable liposome formulations like Arikace® are considered the first generation 543 of inhalable liposome medicines, liposomal and proliposomal DPIs might constitute the second-544 545 generation formulations. The proliposome formulations introduced in this study offer the rationale of 546 delivering small therapeutic doses of SS with relatively small doses of phospholipid and sugar; this 547 may reduce the risk of 'overwhelming' the lung with large amounts of exogenous lipids. Future 548 investigations should expand to explore the role of materials used to manufacture the capsules that 549 accommodate the powder prior to loading into the inhaler device $(\underline{82})$, and the role of inhaler device design (83, 84), aiming to maximize formulation output and FPF. Importantly, aerosol flow rate 550 from DPI devices may affect the deposition profile for conventional powders (85); thus, studying 551 the role of flow rate through an impinger and its influence on the emitted dose and FPF is part of our 552 ongoing investigations using phospholipid-based powders. Finally yet importantly, in vivo studies 553 554 using experimental animals are needed in the future to further explore the potential of DPI 555 proliposomes for inhalation to treat pulmonary diseases (e.g. asthma).

557 4. Conclusions

In this study, novel spray-dried proliposome formulations for delivery as dry powders were 558 559 investigated using LMH or mannitol as carriers and SPC and CH as lipid composition. The ratio of carrier to lipid has influenced the product yield, particle morphology, and powder crystallinity and 560 deposition pattern in the TSI. The characteristics of proliposome microparticles have accordingly 561 562 influenced the vesicles generated, in terms of size, surface charge and drug entrapment. The 563 production yield of spray-dried LMH formulations was higher than the yield values shown for mannitol-based proliposomes. X-ray diffraction patterns demonstrated the crystallinity of 564 proliposomes after spray drying from ethanolic suspensions, indicating interaction between the 565 566 proliposome constituents. SEM, impinger investigations, and powder floewability studies showed mannitol to be a more appropriate carrier for manufacturing DPI proliposome formulations because 567 568 its particles were spherical, smooth and small after spray drying, and offered higher 'FPF' using the 569 TSI (exceeding 50%). By contrast, LMH-based proliposomes were irregular in shape, had rough 570 surfaces, larger sizes and poorer flowability, compromising its suitability for as DPI formulations. 571 However, the vesicles generated upon hydration of proliposomes using LMH carrier offered higher 572 drug entrapment efficiencies. The higher drug entrapment in liposomes generated from LMH-based 573 formulations can be ascribed to the larger size of vesicles generated using this carrier. The zeta 574 potential values were slightly negative, regardless of formulation composition. Moreover, TEM 575 showed that mannitol-based proliposomes generated spherical vesicles, while bilayer structures generated upon hydration of LMH-based proliposomes were "worm-like" clusters. Following on the 576 advanced development stages achieved by nebulizable liposome dispersions for inhalation, we expect 577 phospholipid-based dry powders delivered via DPI devices, similar to the formulations developed in 578 this study, to constitute the second generation of inhalable liposomes. 579

581 5. Acknowledgements

- 582 We thank MIAT, Italy for supplying us with the Monodose dry powder inhaler device. We also thank
- 583 Mr. David McCarthy, Microscopy unit, UCL-School of Pharmacy for the TEM images, and Lipoid,
- 584 Switzerland for supplying us with SPC (Lipoid S-100).
- 585

586 6. Conflict of interests

- 587 The authors of this manuscript declare no conflict of interests.
- 588

589 7. References

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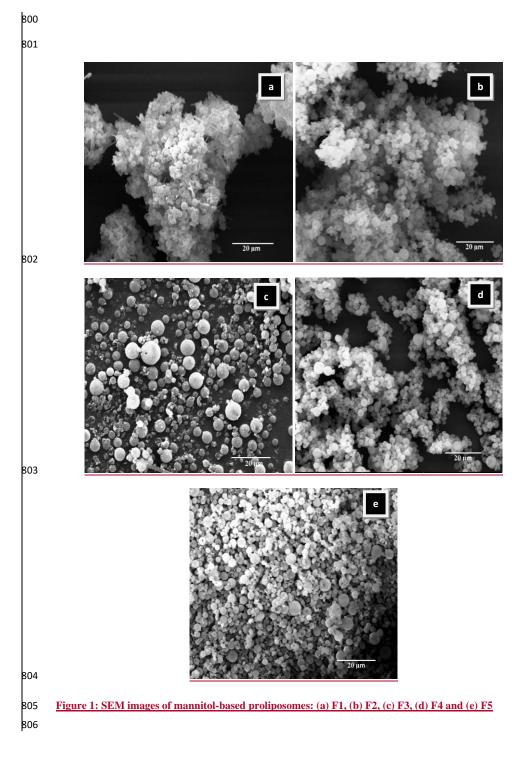
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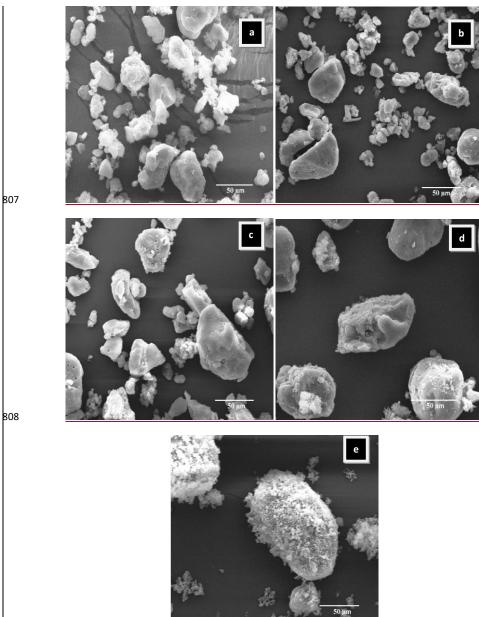
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Formulation	Lipid : Carrier	Lipids (SPC:CH; 1:1)	<u>Mannitol</u>	<u>LMH</u>	<u>SS</u>
	<u>(w/w)</u>	<u>(mg)</u>	<u>(mg)</u>	<u>(mg)</u>	<u>(mg)</u>
<u>F1</u>	<u>1:2</u>	<u>100</u>	<u>200</u>	± 1	<u>10</u>
<u>F2</u>	<u>1:4</u>	<u>100</u>	<u>400</u>	=	<u>10</u>
<u>F3</u>	<u>1:6</u>	<u>100</u>	<u>600</u>	Ξ	<u>10</u>
<u>F4</u>	<u>1:8</u>	<u>100</u>	<u>800</u>	± 1	<u>10</u>
<u>F5</u>	<u>1:10</u>	<u>100</u>	<u>1000</u>	Ξ	<u>10</u>
<u>F6</u>	<u>1:2</u>	<u>100</u>		200	<u>10</u>
<u>F7</u>	<u>1:4</u>	<u>100</u>	=	<u>400</u>	<u>10</u>
<u>F8</u>	<u>1:6</u>	<u>100</u>	=	<u>600</u>	<u>10</u>
<u>F9</u>	<u>1:8</u>	<u>100</u>		<u>800</u>	<u>10</u>
<u>F10</u>	<u>1:10</u>	<u>100</u>	=	1000	<u>10</u>

797 <u>Table 1: Composition of the proliposome formulations manufactured using spray drying</u>



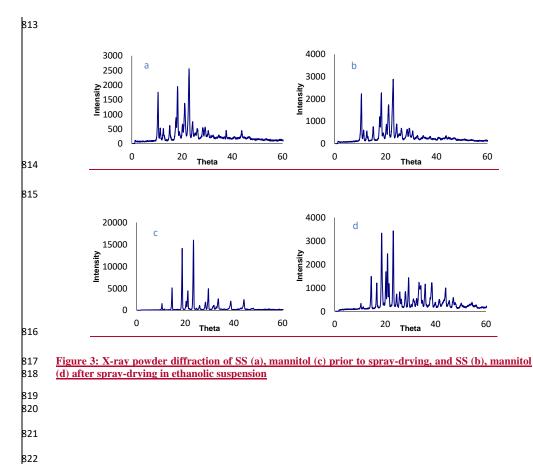
Spray-dried proliposomes for aerosol delivery

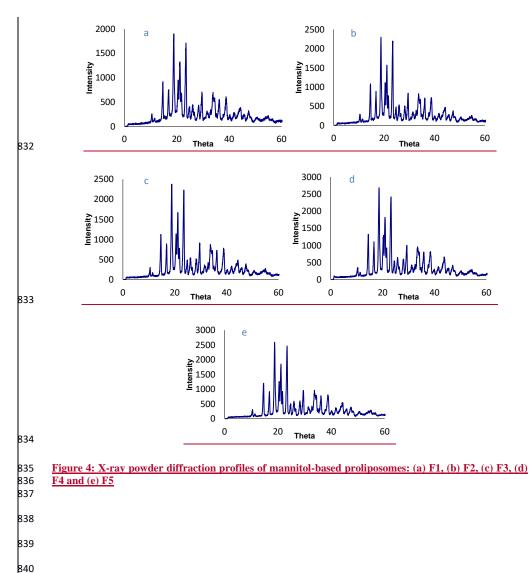


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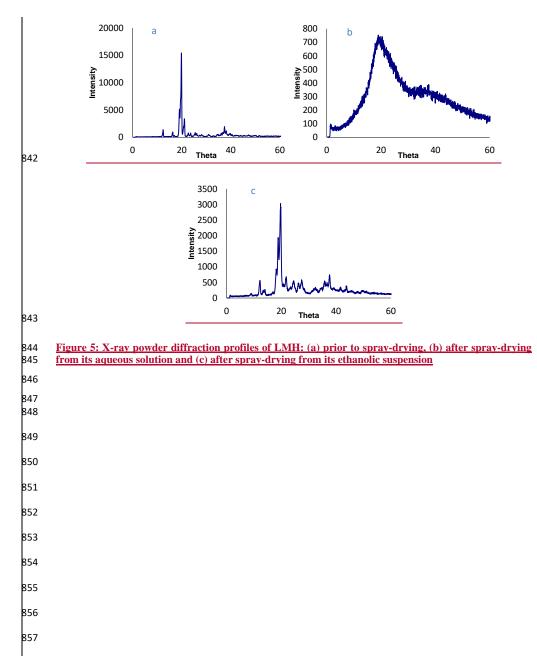
Figure 2: SEM images of LMH-based proliposome formulations: (a) F6, (b) F7, (c) F8, (d) F9 and (e) F10

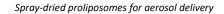
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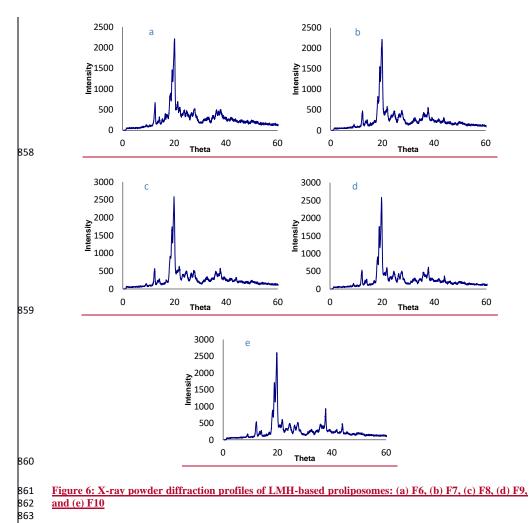




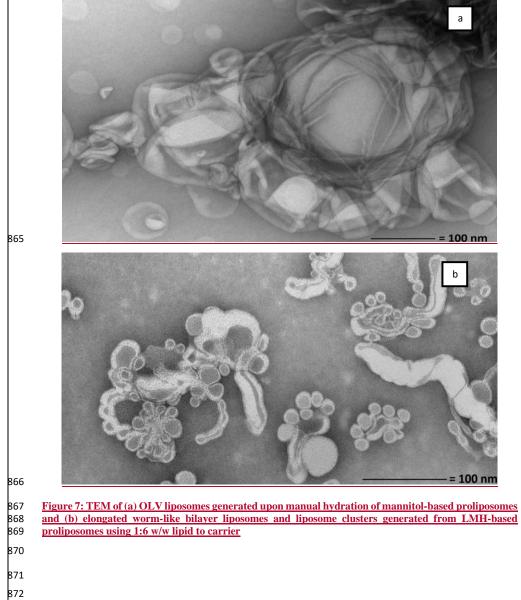








Spray-dried proliposomes for aerosol delivery



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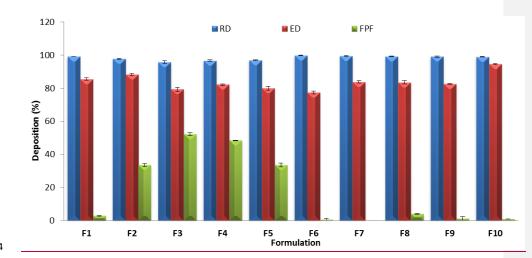
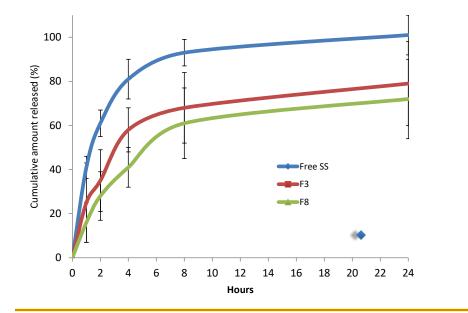


Figure 8: Recovered dose (RD; %), emitted dose (ED; %) and 'fine particle fraction' ('FPF'; %) of mannitol-based and LMH-based proliposomes (n = 3 ± SD)

Spray-dried proliposomes for aerosol delivery



<u>Figure 9: Drug release profile from liposomes generated from mannitol-based proliposomes</u> (F3) and LMH-proliposomes (F8) in comparison to free SS ($n = 3 \pm SD$)